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Sustainable Engineering and Eco Design

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1. Introduction

The material consumption in the United States of America now exceeds ten tones per person per year. The average level of global consumption is about eight times smaller than this but is growing twice as fast. The materials and the energy needed to make and shape them are drawn from natural resources: ore bodies, mineral deposits, and fossil hydrocarbons. The demand of natural resources throughout the 18th, 19th and early 20th century appeared infinitesimal (Ashby et al., 2007, Alonso et al., 2007, Chapman and Roberts, 1983, and Wolfe, 1984). There is also a link between the population growth and resource depletion (Ashby et al., 2007, Alonso et al., 2007, Chapman and Roberts, 1983, and Wolfe, 1984). The global resource depletion scales with the population and with per-capita consumption (Ashby et al., 2007, and Alonso et al., 2007). Per capita consumption is growing more quickly.

The first concern is the resource consumption. Speaking globally, we consume roughly 10 billion tones of engineering materials per year. We currently consume about 9 billion tones per year of hydrocarbon fuels (oil and coal). For metals, it appears that the consumption of steel is the number one (~ 0.8 billion tones per year) followed by aluminum (10 millions tones per year). The consumption of steel exceeds, by a factor of ten all other metals combined. Polymers come next: today the combined consumption of commodity polymers polyethylene (PE), polyvinyl chloride (PVC), polypropylene (PP) and polyethylene-terephthalate, (PET) begins to approach that of steel (see figure 1). The really big ones, though, are the materials of the construction industry. Steel is one of these, but the consumption of wood for construction exceeds that of steel even when measured in tones per year, and since it is a factor of 10 lighter, if measured in m3/year, wood totally eclipses steel. Bigger still is the consumption of concrete, which exceeds that of all other materials combined as shown in Figure 1. The other big ones are asphalt (roads) and glass.

The second concern is the energy and carbon release to atmosphere caused by the production of these materials as shown in Figure 2. This is calculated by multiplying the annual production by the embodied energy of the material (MJ/Kg – energy consumed to make 1 Kg of material). During the primary production of some materials such as metals, polymers, composites, and foams the embodied energy is more than 100 MJ/Kg and the CO2 foot print exceeds 10 Kg of CO2 per Kg of materials.

New tools are needed to analyze these problems (high resource consumption, energy use and CO2 emissions) best material based on the design requiment but also to reduce the environmental impacts.

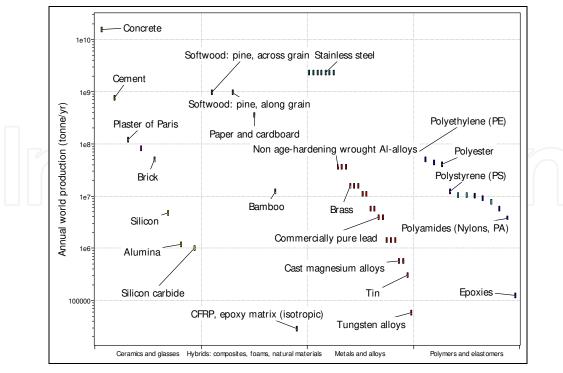


Fig. 1. Annual world production for principal materials

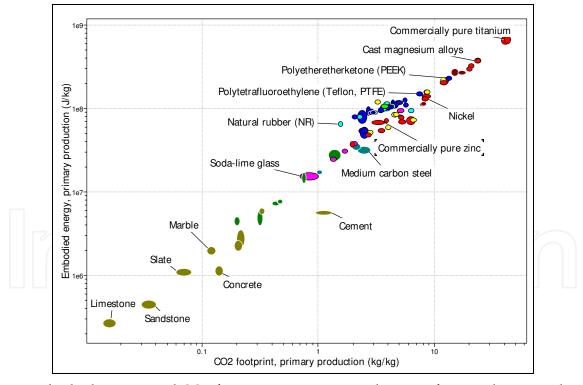


Fig. 2. Embodied Energy and CO2 footprint - primary production of principle materials

To select an eco friendly and sustainable material, one need to examine first the materials life cycle and consider how to apply life cycle analysis (Ashby et al., 2007). The materials life cycle is sketched in Figure 3. Ore and feedstock are mined and processed to yield materials. These materials are manufactured into products that are used and at the end of life,

discarded, recycled or (less commonly) refurbished and reused. Energy and materials are consumed in each phase (material, manufacturing, use, transportation and disposal) of life, generating waste heat and solid, liquid, and gaseous emissions (Ashby et al., 2007). The results of the eco audit or life cycle analysis is shown in Figure 4. The results of the life cycle analysis will reveal the dominant phase that is consuming more energy or producing high CO2 emission. The next step is to separate the contributions of the phases of life because subsequent action depends on which is the dominant one. If it is that a material production, then choosing a material with low embodied energy is the way forward. But if it is the use phase, then choosing a material to make use less energy-intensive is the right approach – even if it has a higher embodied energy.

This chapter introduces the methods and tools that will guide in the design analysis of the role of materials and processes selection in terms of embodied energy, carbon foot print, recycle fraction, toxicity and sustainability criteria. A particular skills need to be used by engineer or designer to guide design decisions that minimize or eliminate adverse eco impacts. Methods and tools that will guide in the design analysis of the role of materials and processes selection in terms of embodied energy, carbon foot print, recycle fraction, toxicity and sustainability criteria need to be used during the design process. Topics covered in this chapter will include: resource consumption and its drivers, materials of engineering, material property charts, the material life cycle, eco data, eco-informed material selection, and eco audits or life cycle analysis. The Cambridge Engineering Selecor software (Granta Design Limited, 2009) is used in this study for better understanding of these issues, create

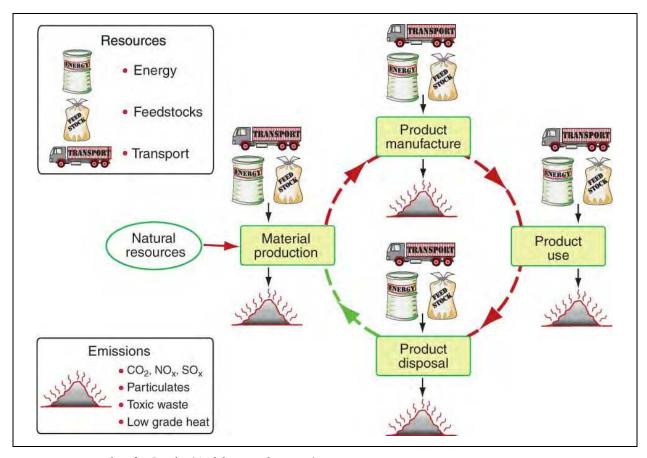


Fig. 3. Material Life Cycle (Ashby et al., 2007)

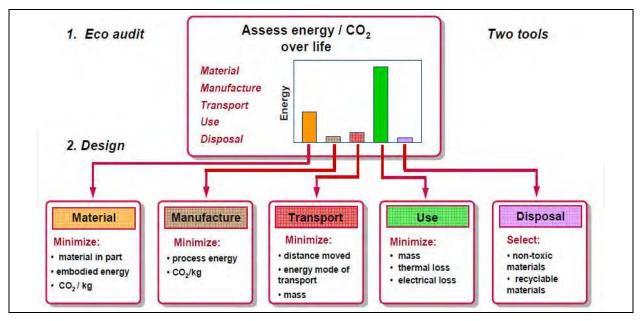


Fig. 4. Eco Audit and Eco Design (Ashby et al., 2007)

material charts, perform materials and processes selection, and eco audit or life cycle analysis allowing alternative design choices to meet the engineering requirements and reduce the environmental burden. The results of two case studies (material selection of desalination plant heat exchanger and life cycle analysis of patio heater) will be presented in this chapter book.

2. Material and process families and eco data

The common material properties are: general properties (cost and density), mechanical properties (strength, stiffness, toughness), thermal properties (conductivity, diffusivity, expansion, heat capacity), electrical properties (electrical conductivity, dielectric constant), optical (refraction, absorption), magnetic, and chemical properties (corrosion resistance). Materials properties determine the suitability of a material based on design requirements. A successful product, one that performs well, is good value for money and gives pleasure to the user uses the best materials for the job, and fully exploits its potential and characteristics. Materials selection is not about choosing a material, but a profile of properties that best meets the needs of the design (Ashby et al., 2007, and Alonso et al., 2007). Material and process are interdependent and grouped into families; each family has a characteristic profile (family likeness) which is useful to know when selecting which family to use for a design. In general, there are six families for materials (Ashby, 2005): metals (steels, cast alloys...), ceramics (alumina, silicon carbides), polymers (polyethylene, polypropylene, polyethylene-terephthalate), glasses (soda glass, borosilicate glass), elastomers (isoprene, neoprene, butyl rubber, natural rubber) and hybrids (composites, foams) as shown in Figure 5.

Processes are also classified based on the design requirements (material, shape, dimensions, precision, and the number of parts to be made). The process families (Ashby, 2005) are: shaping (casting, molding, deformation, machining, heat treatment), joining (fastening, welding, adhesives) and surface treatments (polishing, painting) as shown in Figure 6.

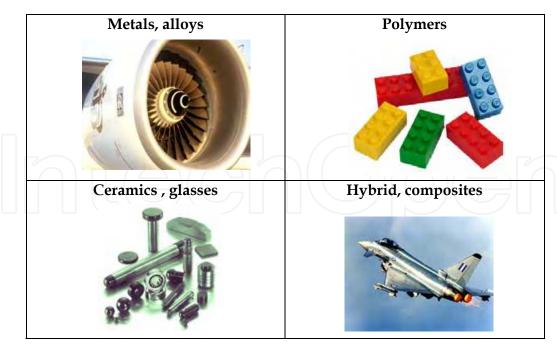


Fig. 5. Materials Families

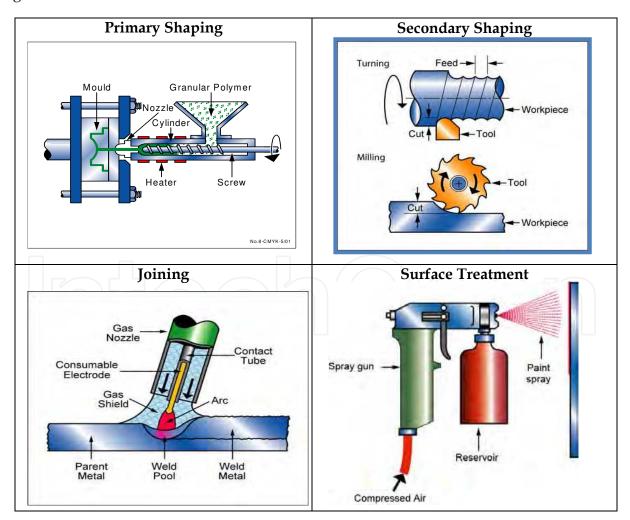


Fig. 6. Process Families

The material and process selection based on some design requirements rely on the materials mechanical, thermal, electrical and chemical properties. Rational selection of materials to meet environmental objectives starts by identifying the phase of product-life that causes greatest concern: production, manufacture, use or disposal. Dealing with all of these requires data for the obvious eco-attributes such as energy, CO2 (Chapman, 1983) and other emissions, toxicity, ability to be recycled and the like (see table 1). Thus if material production is the phase of concern, selection is based on minimizing production energy or the associated emissions (CO2 production for example). But if it is the use-phase that is of concern, selection is based instead on light weight, excellence as a thermal insulator, or as an electrical conductor (while meeting other constraints on stiffness, strength, cost etc). Additional information such eco data (embodied energy and CO2 foot print as shown in Figure 2 and table 1) is needed for sustainable engineering and eco design.

Geo-Economic Data for Principal Component

Annual world production	21e6-23e6	tonne/year
Reserves	2e10 - 2.2e10	tonne
Typical exploited ore grade	30 - 34	%

Material Production - Energy and Emissions

Production energy	190 - 210	MJ/Kg
CO2	12-13	kg/kg
NOX	72-79	g/kg
SOX	120- 140	g/kg

Indicators for Principal Component

Eco indicator	740 - 820	mmillions points/kg
---------------	-----------	---------------------

End of life

Recycle	True	
Down cycle	True	
Biodegrade	False	
Incinerate	False	
Landfill	True	
Recycle as fraction	34 - 38	%

Bio Data

Toxicity rating	Non toxic	
Approve for skin and food	True	
contact		

Sustainability

Sustainable material	No	

Table 1. Eco Data - Wrought Aluminium Pure

3. Life cycle analysis and selection strategies

The material life cycle is shown in Figure 3. Ore and feedstock, drawn from the earth's resources, are processed to give materials. These materials are manufactured into products that are used, and, at the end of their lives, discarded, a fraction perhaps entering a recycling loop, the rest committed to incineration or land-fill (Gabi, 2008, Graedel, 1998, and Kickel, 2009) Energy and materials are consumed at each point in this cycle (phases), with an associated penalty of CO2, SOx, NOx and other emissions, heat, and gaseous, liquid and solid waste. These are assessed by the technique of life-cycle analysis (LCA) (Ashby, 2007).

3.1 The steps for life cycle analysis are:

- 1. Define the goal and scope of the assessment: Why the assessment needs to be done? What is the subject and which part of its life are assessed?
- 2. Compile an inventory of relevant inputs and outputs: What resources are consumed? (bill of materials) What are the emissions generated?
- 3. Evaluate the potential impacts associated with those inputs and outputs
- 4. Interpretation of the results of the inventory analysis and impact assessment phases in relation of the objectives of the study: What the result means? What needs to be done about them?

The study examine the energy and material flows in raw material acquisition; processing and manufacturing; distribution and storage (transport, refrigeration...); use; maintenance and repair; and recycling options.

3.2 The strategy for guiding design

The first step is to develop a tool that is approximate but retains sufficient discrimination to differentiate between alternative choices. A spectrum of levels of analysis exist, ranging from a simple eco-screening against a list of banned or undesirable materials and processes to a full life cycle analysis, with overheads of time and cost.

The second step is to select a single measure of eco-stress. On one point there is some international agreement: the Kyoto Protocol of 1997 committed the developed nations that signed it to progressively reduce carbon emissions, meaning CO2 (Kyoto Protocol, 1999). At the national level the focus is more on reducing energy consumption, but since the energy consumption and CO2 production are closely related, they are nearly equivalent. Thus there is certain logic in basing design decisions on energy consumption or CO2 generation; they carry more conviction than the use of a more obscure indicator. We shall follow this route, using energy as our measure.

The third step is to separate the contributions of the phases (material, manufacturing, use, transportation and disposal) of life because subsequent action depends on which is the dominant one with respect of energy consumption and CO2 emissions (see Figure 4).

For selection to minimize eco-impact we must first ask: which phase of the life cycle of the product under consideration makes the largest impact on the environment? The answer guides material selection. To carry out an eco-audit or life cycle analysis we need the bill of material, shaping or manufacturing process, transportation used of the parts of the final product, the duty cycle during the use of the product, and also the eco data for the energy and CO2 footprints of materials and manufacturing process.

4. Results

Two case studies of sustainable engineering and eco design are presented in this chapter book. The first case study deals with material selection for the condenser used in desalination plant (sustainable material). The question is what is the best material that can be used for the condenser based on some constraints and design objectives? The second case study is about the life cycle analysis of patio heater. The question is what the dominant phase of the life cycle of this product that is consuming more energy and producing more CO2 emissions?

4.1 Case study 1: Material selection for desalination plant heat exchanger

Desalination of seawater is one of the most promising techniques used to overcome water shortage problems (Nafey et al., 2004). The desalination techniques include thermal desalination processes (Multi Stage Flash - MSF, Multi Effect Distillation - MED) and membrane desalination processes (reverse osmosis - RO and Electro-Dialysis Reverse -EDR). Multi Stage Flash (MSF) is one of he most commonly distillation process used for large-scale desalination of seawater (Hassan, 2003). In the MSF process, the seawater enters the evaporation chamber resulting in flash boiling of a fraction of the seawater. The vapour produced by flashing is then conveyed to the heat recovery section where it is condensed. Heat exchanger (evaporator and condensers) tubes represent the largest item in an MSF plant and not surprisingly more than 70% of the corrosion failures in desalination plants are attributed to heat exchange tubes. Heat exchangers tubes handle two fluids of completely different properties (seawater and vapors). It is one of the severest environments from the point of view of corrosion (Anees et al., 1993, and Aness et al., 1992). This study focuses only on the desalination plant condensers. The condenser is a sea water-cooled shell and tube heat exchanger installed in the exhaust steam from the evaporator in thermal desalination plant. The condenser is a heat exchanger that converts the steam received from the evaporator to liquid using the sea water as the cooling fluid. The key properties of the desalination plant surface condenser are: (1) heat transfer properties (thermal conductivity, convective heat transfer coefficients for steam and sea water, and fouling coefficients); (2) the erosion resistance (to steam for the external surface of the tube, and to raw sea waters which may contain sand and show turbulences for the internal surface of the tube); (3) corrosion resistance (to raw sea waters, steam and condensate). The heat transfer performance of the condenser is linked to the material selection - thermal conductivity, thickness, and the erosion/corrosion resistance of the tubing materials.

A condenser with high tubing thermal conductivity, thin wall tubing, and tubing surface that do not corrode in the heat exchanger environment and remains relatively cleans during the desalination process will provide excellent heat transfer performance. The principal objective of this study is to select the best materials for the condenser tubing (sustainable material) that will provide excellent thermal heat transfer performance, low cost and low embodied energy (sustainable energy) and CO2 foot print (sustainable environment).

The condenser shown in Figure 7 takes heat from the steam and passes it to the sea cooling water. The steam enters the shell at temperature T_V , changes its phase from gas to liquid during the heat transfer with the sea cooling water and exit the heat exchanger as condensate at temperature T_C . The sea water cooling fluid enters the condenser tubes at

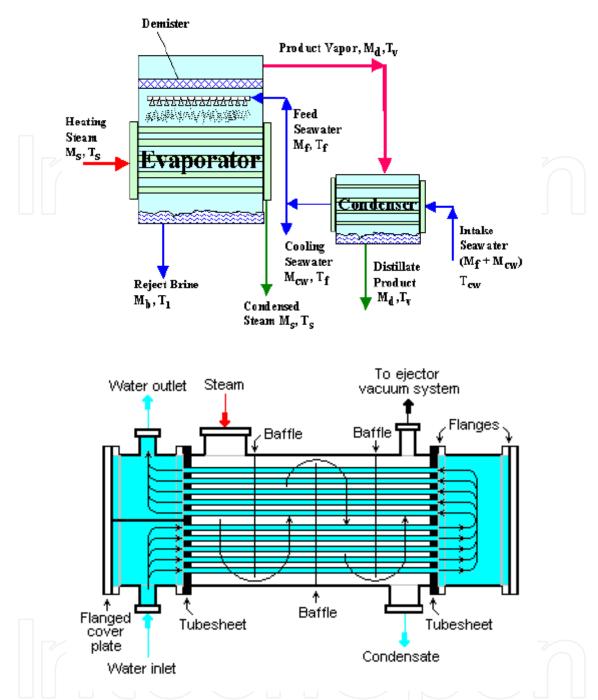


Fig. 7. Desalination process and heat exchanger (condenser)

temperature T_{CW} and exit at high temperature T_{HW} . A key element in all heat exchangers is the tube wall or membrane which separates the sea water and the steam. It is required to transmit heat and there is frequently a pressure difference across it Δp (pressure difference between the sea water and the steam pressures). The question is what are the best materials for making these condensers? What are the best condenser materials that can provide high thermal conductivity but at the same time can sustain this pressure difference? What is the performance index that can be use for heat exchanger or condensers? The heat transfer from the steam to the sea water through the membrane or the thin wall involves convective transfer from steam to outside surface of the condenser tubes, conduction through the tube

wall, and convection again to transfer the heat to sea water. The heat flux q into the tube wall by convection (W/m²) is described by the heat transfer equation $q = h_1 \Delta T_1$, where h1 is the heat transfer coefficient for the steam and $\Delta T1$ is the temperature drop across the surface from the steam into the outside tube wall. Conduction is described by the conduction equation; $q = (\lambda \Delta T_{12})/e$, where λ is the thermal conductivity of the wall (thickness e) and $\Delta T12$ is the temperature difference across the tube wall. The heat flux q out from the tube wall by convection is described by the heat transfer equation $q = h_2 \Delta T_2$, where h_2 is the heat transfer coefficient for sea water and ΔT_2 is the temperature drop from the inside surface of the tube to the sea water. The heat flux is also given by: $q = U (T_V - T_{CW})$, where U is the overall heat transfer coefficient and T_V is the steam temperature entering the shell and T_{CW} is the temperature of sea water entering the tube. The overall heat transfer coefficient is given by:

$$U = \frac{1}{\frac{1}{h_1} + \frac{e}{\lambda} + \frac{1}{h_2}} \tag{1}$$

The total heat flow is given by:

$$Q = q A = \left(\frac{1}{\frac{1}{h_1} + \frac{e}{\lambda} + \frac{1}{h_2}}\right) A \quad (T_V - T_{CW})$$
 (2)

One of the constraints of the heat exchanger is that the wall thickness must be sufficient to support the pressure difference Δp . This requires that the stress in the wall remain below the elastic limit (yield strength): $\sigma = \frac{\Delta p \ r}{e} \langle \sigma_{el} .$

Where r is the pipe radius and e is the pipe thickness.

The heat flux is given by:

$$\frac{Q}{A} = q = \left(\frac{1}{\frac{1}{h_1} + \frac{\Delta p \, r}{\lambda \, \sigma_{el}} + \frac{1}{h_2}}\right) \quad (T_V - T_{CW}) \tag{3}$$

The heat flow per unit area of tube wall, Q/A or q is maximized by maximizing the performance index M given by $M = \lambda \sigma_{el}$. The maximum value of M is obtained by minimizing the tube wall thickness or maximizing both the thermal conductivity and the yield strength.

Selecting materials for desalination plant heat exchanger involves seeking the best match between design requirements and the properties of the materials that may be used to make the heat exchanger. The strategy for selecting the material for desalination plant heat exchangers is:

- a. Translate design requirements: develop a list of requirements the material must meet, expressed as function (what does the system do), objectives (what is to be maximized or minimized), constraints (what nonnegotiable conditions must met) and free variables (what parameters of the problem is the designer free to change). The main function of the condenser is to exchange heat between the steam and seat water (heat exchanger) and to convert the steam to distilled water. The objectives are to maximize heat flow per unit area, minimize the cost and eco friendly materials (minimize the energy and the CO2 footprint). The constraints for the condenser are: (a) operating temperature up to 150°C; (b) support pressure difference Δp, (c) excellent resistance to sea water, (d) very high resistance of the material to pitting and crevice corrosion, and (e) excellent resistance of the material stress corrosion cracking. The free choices for the condenser design are the choice of material.
- Screening: After developing the list of requirements the material must meet, the next step is to eliminate the materials that can not do the job because one or more their attributes lies outside the limits set by the constraints. The limit and tree stages of the Cambridge selector software (Granta Design Limited, 2009) are used in this study as selection tools for the screening process. The limit stage applies numeric and discrete constraint. Required lower or upper limits for material properties are entered into the limit stage property boxes. If a constraint is entered in the minimum box, only materials with values greater than the constraint are retained. If it is entered in the Maximum box, only materials with smaller values are retained. The graph option can be used to create bar charts and bubble charts. A box selection isolates a chosen part of a chart. Any material bar or bubble lying in, or overlapping the box is selected and all others are rejected. The line selection divides a bubble chart into two regions. The user is free to choose the slope of the line, and to select the side on which materials are to be chosen. This allows selection of materials with given values of combinations of material properties such as E/ρ , where E is Young's modulus and ρ is density. The tree stage allows the search to be limited to either: a subset of materials (metals, hybrids, polymers, and ceramics) or materials that can be processes in chosen ways (manufacturing process).
- c. Ranking: Find the screening materials that do the job best. Rank the materials that survive the screening using the criteria of excellence or the objectives and make the final materials choice.

Figure 8 shows the results of the screening process for the performance index M. Only 16 materials passed the test based on the design requirements (operating temperature > 150 C, resistance to sea water, resistance to pitting and crevice corrosion, and excellent resistance to stress corrosion cracking). Based on the objectives (maximize heat flux, minimize the cost, the embodied energy and CO2 foot print) set during the design process, it is clear that the best material that can be used for the desalination plant condenser is the stainless steel duplex UNS S32550, wrought. It has the maximum value for performance index M (high thermal conductivity and thin tube wall), and lowest cost (14-14 \$/Kg) as shown in Figure 8. In addition to that this material has the lowest embodied energy and CO2 foot print as shown in Figure 9. The characteristics of the selected material for the desalination plant condenser are summarized in Table 2.

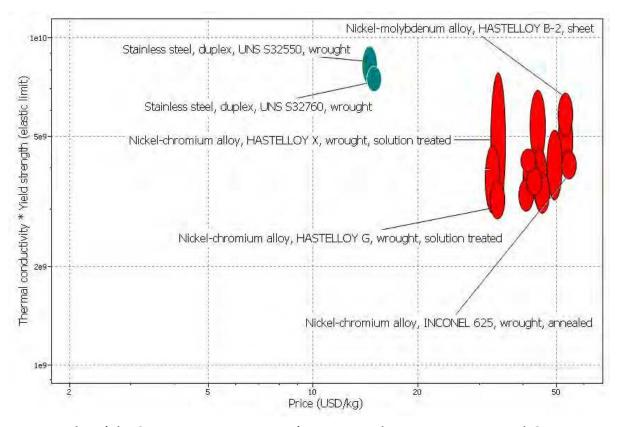


Fig. 8. Results of the Screening Process - Performance Index M versus Material Cost

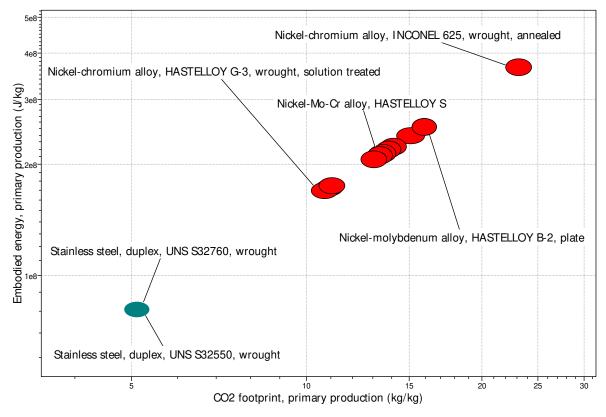


Fig. 9. Results of the Screening Process - Embodied Energy versus the CO2 foot print

Material	Performance Design $M = \lambda \sigma_{el}$	Price \$/Kg	Pitting and Crevice Corrosion	Stress Corrosion Cracking	Embodied Energy (J/Kg)	Maximum Service Temp. (C)
1. Stainless Steel, Duplex UNS S32550, wrought	7.3e9 – 9.4e9	13.2 - 15.2	Very High	Excellent	7.7e7 - 8.5e7	335 – 365
2. Stainless Steel, Duplex UNS S32760, wrought	6.9e9 - 8.1e9	14.2 - 15.7	Very High	Excellent	7.7e7 - 8.5e7	335 – 365

Table 2. Selected Materials for the desalination plant condenser

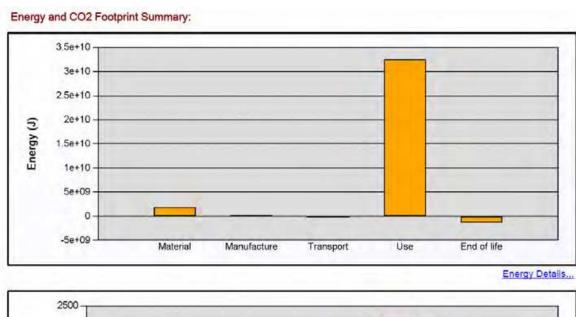
4.2 Case Study 2: Life cycle analysis of patio heater

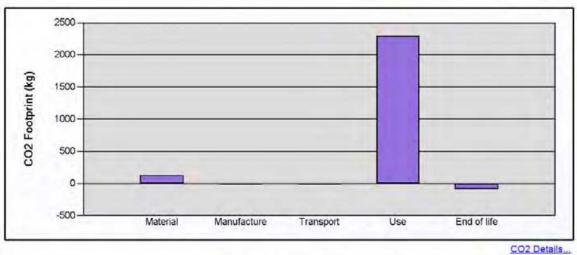
An eco audit is a fast initial assessment. It identifies the phases of life – material, manufacture, transport, and use – that carry the highest demand for energy or create the greatest burden of emissions. It points the finger, so to speak, identifying where the greatest gains might be made. Often, one phase of life is, in eco terms, overwhelmingly dominant, accounting for 60% or more of the energy and carbon totals. This difference is so large that the imprecision in the data and the ambiguities in the modeling, are not an issue; the dominance remains even when the most extreme values are used. It then makes sense to focus first on this dominant phase, since it is here that the potential innovative material choice to reduce energy and carbon are greatest.

An energy and CO2 eco audits were performed for the patio heater shown in Figure 10. It is manufactured in Southeast Asia and shipped 8,000 Km to the United States, where it is sold and used. It weighs 24 kg, of which 17 kg is rolled stainless steel, 6 kg is rolled carbon steel, 0.6 kg is cast brass and 0.4 kg is unidentified injection-molded plastic (See Materials - Tables 3 and 4). During the use, it delivers 14 kW of heat ("enough to keep 8 people warm") consuming 0.9 kg of propane gas (LPG) per hour, releasing 0.059 kg of CO2 /MJ.

The heater is used for 3 hours per day for 30 days per year, over 5 years, at which time the owner tires of it and takes it to the recycling depot (only 6 miles / 10 km away, so neglect the transport CO2) where the stainless steel, carbon steel and brass are sent for recycling (See end of life - Tables 3 and 4). These data are used to construct a bar-chart for energy and CO2 emission over the life of the patio heater.

The table (See Figure 10) lists the energy and carbon footprints of the materials and manufacturing processes for the patio heater. The bar chart plots the totals for each phase. For the sea transport over 8000km, the energy consumed is 30.7 MJ and the CO2 released is 2.18 kg of carbon dioxide, so small as to be invisible on the bar chart. The results show that 97.9% of the energy consumed and 98.1 % of the CO2 emitted are during the use phase. The energy consumed and CO2 emitted for the material phase are respectively 5.9% and 5.2%. The results also show that 4.1% of the energy can be recovered and 3.7 % reduction of CO2 emission can be obtained by recycling the parts of the patio heater. A detailed breakdown of the energy and CO2 foot print for individual life phases (material, manufacture, transport, use, and end of life) are shown respectively in Tables 3 and 4.





Phase	Energy (J)	Energy (%)	CO2 (kg)	CO2 (%)
Material	1.94e+09	5.9	123	5.2
Manufacture	8.41e+07	0.3	6.7	0.3
Transport	3.07e+07	0.1	2.18	0.1
Use	3.24e+10	97,9	2.3e+03	98.1
End of life	-1.36e+09	-4.1	-86.2	-3.7
Total	3.31e+10	100	2.35e+03	100



Fig. 10. Life Cycle Analysis of Patio Heater: Energy and CO2 Footprint Analysis

	Breakdown by compo	onent			1	Aller Co.		
	Component	Mater	rial	Recycle content	Embodi Energy (J/kg)	d Total	Energy (J)	%
	Component 1	Stainless ster		Virgin (0%)	8,1e+0	7 17	1.4e+09	71.1
Material	Component 2	Stainless martensitic, A 15, cast, ten 315°	steel. ASTM CA- npered at	Virgin (0%)	8.1e+0	7 6	4,9e+D8	25,1
	Compoent 3	Brass, CuZn1	10Pb3Sn2,	Virgin (0%)	7e+07	0.6	4.2e+07	2.2
	Component 4	PP (65-70%	6 barium	Virgin (0%)	7.7e+0	7 0.4	3.1e+07	1.6
	Total	sulfat	(e)			24	1.9e+09	100
	Breakdown by comp	onent						
	Component	Pi	rocess		cessing	Total Mass (kg)	Energy (J)	%
	Component 1	Forg	Forging, rolling		2.9e+05		5e+07	59.6
Manufacture	Component 2	Forgi	ing, rolling	- 4	1e+06	6	2.5e+07	29.5
	Compoent 3		asting		.7e+05	0.6	1.6e+06	1.9
	Component 4	Polym	ser molding	1	9e+07	0,4	7.6e+06 8.4e+07	9.0
					29	24	0.49707	100
	Breakdown by transp	ort stage Total	product	mass = 24 l	ansport			
	Stage Name	Trans	port Type	E	nergy	Distance (m)	Energy (J)	%
		Sec	a freight	- 1	(kg.m) 0.16	8e+06	3.1e+07	100.
	Total					8e+06	3.1e+07	100
Transport	Breakdown by compo	nents Total	transpor	t distance =	8e+06 m			
Transport	Component		Mass (kg)	Committee of the last of the l	ergy (J)	%		
	Component 1		17	2	2e+07	70.8		
	Component 2		6	_	7e+06	25.0		
	Compoent 3	0.6		7.7e+05		2.5		
	The state of the s							
	Component 4 Total Relative contrib		0.4 24 c and n	3	.1e+05 .1e+07	1.7		
	Total		24	nobile m	1e+05 1e+07 odes	1.7	%	
	Relative contrib		24	3	1e+05 1e+07 odes y (J)	1.7	% 100.0	-
	Relative contrib		24	nobile m	1e+05 1e+07 odes y (J)	1.7		
	Relative contrib		24	nobile m Energ	1e+05 .1e+07 odes y (J)	1.7		
Use	Relative contrib		24	nobile m Energ 3.2e-	1e+05 .1e+07 odes y (J)	1.7	100.0	
Use	Relative contrib	oution of statio	c and n	nobile m Energ 3.2e-	odes y (J):-10	1.7	100.0	
Use	Relative contrib	oution of statio	c and n	nobile m Energ 3.2e-	odes y (J):-10	1.7	100.0	
Use	Relative contrib	oution of statio	c and n	3.2e-	odes y(J) -10 -10 -10 -10 -10	1.7	100.0	
Use	Relative contrib	oution of statio	c and n	Energ 3.2e- 0 3.2e- fuel to therrited system 0.7	odes y(J) -10 -10 -10 -10 -10	1.7	100.0	
Use	Relative contrib	oution of statio	c and n	Energ 3.2e- 0 3.2e- fuel to therrited system 0.7	odes y(J) -10 -10 -10 -10 -10	1.7	100.0	
Use	Relative contrib	oution of statio	c and n	3.2e- 3.2e- 0 3.2e- fuel to them ted system 0.7 ited States	odes y(J) -10 -10 -10 -10 -10	1.7	100.0	
Use	Relative contrib	oution of station output Type e, source (J/J)	c and n	nobile m Energ 3.2e- 0 3.2e- fuel to them ted system 0.7 ited States 1 14	odes y(J) -10 -10 -10 -10 -10	1.7	100.0	
Use	Relative contrib	oution of station of s	c and n	snobile m Energ 3.2e- 0 3.2e- fuel to thereted system 0.7 ited States 1 14 3	odes y(J) -10 -10 -10 -10 -10	1.7	100.0	
Use	Relative contrib	oution of station output Type e, source (J/J) ay)	Fossil t	fuel to therrited system 0.7 ited States 1 14 3 30 5	odes y(J) -10 -10 -10 -10 -10	1.7	100.0	
Use	Relative contrib	oution of station of s	Fossil 1 ven	fuel to therrited system 0.7 ited States 1 14 3 30	odes y(J) -10 -10 -10 -10 -10	1.7	100.0	
	Relative contrib	oution of station of s	Fossil 1 ven	fuel to therrited system 0.7 ited States 1 14 3 30 5	odes y(J) 10 10 10 10 10 10 10 10	1.7 100	100.0	%
nţ	Relative contrib	e, source (J/J) ay) ar) urs) s of end of life op	Fossil 1 ven	3.2e- fuel to them ted system 0.7 ited States 1 14 3 30 5 4.5e+02	1e+05 .1e+07 odes y (J) .10 .10 .10 .10 .10 .10 .10 .10 .10 .10	1.7 100	100.0 100	% 71.7
nt	Relative contribution Relative contribution Mode Static Mobile Total Static Mode Energy Input and O Product Efficiency Use Location Energy Equivalence Power Rating (kW) Usage (hours per d Usage (days per ye Product Life (years Total Life Usage (hour Relative contribution Component Component 2	e, source (J/J) ay) ar) burs) s of end of life op	Fossil 1 ven	13.2e+ 0 3.2e+ 0 3.2e+ fuel to themsted system 0.7 ited States 1 14 3 30 5 4.5e+02 Collection Energy (J/kg) 7e+05 7e+05	1e+05 .1e+07 odes y (J) -10 -10 -10 -10 -10 -10 -10 -10 -10 -10	1.7 100 Total Massig (kg) 17	100.0 100 100 Total EoL Energy (J) -9.8e+08	71.7
Use End of Life	Relative contrib	ay) s of end of life opi	Fossil 1 ven	1 3 3 3 3 3 3 3 3 3 3 3 3 3 3 3 3 3 3 3	ne+05 ne+07 odes y (J) -10 Potential Er of Life 'Saving' (J/I) -5.8e+07	1.7 100 Total Mass (kg)	100.0 100 Total EoL. Energy (J) -9.8e+08	, m

 $Table\ 3.\ Detailed\ Breakdown\ of\ individual\ life\ phases:\ \textit{Energy\ Analysis}\ \textbf{-}\ Patio\ Heater$

	Component	Material	Recycl			CO2 Footprint (kg)	%
	Component 1	Stainless steel, duple. ASTM CD-4MCu, cas	X, Virgin (0	COLUMN TO THE PARTY OF THE PART	17	87	70.5
Material	Component 2	Stainless steel, martensitic, ASTM CA 15, cast, tempered a 315°C	A- Virgin /0	%) 5.1	6	31	24.9
	Compoent 3	Brass, CuZn10Pb3Sn sand-cast	2. Virgin (0	%) 6.2	0.6	3.7	3.0
	Component 4	PP (65-70% barium sulfate)	Virgin (01	%) 4.7	0.4	1.9	1.5
	Total	Suilate)			24	1.2e+02	100
		LOWE		110			
	Breakdown by componer	Process		Processing	Total Mass	CO2	
				CO2 (kg/kg)	(kg)	Footprint (kg)	%
Manufacture	Component 1	Forging, rollin		0.24	17	4	59,8
viairaiactare	Component 2	Forging, rollin	9	0.33	6	2	29.6
	Compoent 3	Casting		0,16	0.6	0.097	1.4
	Component 4	Polymer molds	ng	1.5	0.4	0.61 6.7	9.1
	Total				24	6.7	100
	Breakdown by transport	stage Total produc	ct mass = 2	4 kg			
	No. comments	To a substitution of the same of the	Transport	CO2 Footprin	and the second	CO2	0,370
	Stage Name	Transport Type En	ergy (J/kg.m)) Footprint	%
		Sea freight	0.16	7.1e-08	8e+06	(kg)	100.0
	Total	SAN MANGEN	91.19	1,510.00	8e+06	2.2	100
_			100				
Transport	Breakdown by compone	The second second	I a	e = 8e+06 m			
	Component	Total Mass (k	g) C	(kg)	%		
	Component 1	17		1.5	70.8		
	Component 2	6		0.55	25.0		
	Compoent 3	0.6		0.055	2.5		
	Component 4	0.4		0.036	1,7		
	Total	24		2.2	100		
	Relative contribution		ootprint (kg)		%		
	Static Mobile		2.3e+03 0		700.0		
	7.00				100		
Use	Mobile	2	0 2.3e+03	5)			
Use	Mobile Total		0 2,3e+03 thermal.	5			
Use	Mobile Total Static Mode	voe Fossil fuel to	0 2,3e+03 thermal.				
Use	Mobile Total Static Mode Energy Input and Output T	ype Fossii fuel to vented sy:	0 2,3e+03 thermal, stem	5 2			
Use	Mobile Total Static Mode Energy Input and Output T Product Efficiency	ype Fossil fuel to vented sy: 0.7 United St	0 2,3e+03 thermal, stem				
Use	Mobile Total Static Mode Energy Input and Output T Product Efficiency Use Location	ype Fossil fuel to vented sy: 0.7 United St	0 2,3e+03 thermal, stem				
Use	Mobile Total Static Mode Energy Input and Output T Product Efficiency Use Location CO2 Footprint, source (kg)	ype Fossil fuel to vented sy: 0.7 United St	0 2,3e+03 thermal, stem				
Use	Mobile Total Static Mode Energy Input and Output T Product Efficiency Use Location CO2 Footprint, source (kg) Power Rating (kW)	ype Fossil fuel to vented sy: 0.7 United St U) 7.1e-0	0 2,3e+03 thermal, stem				
Use	Mobile Total Static Mode Energy Input and Output T Product Efficiency Use Location CO2 Footprint, source (kg) Power Rating (kW) Usage (hours per day)	ype Fossil fuel to vented sy: 0.7 United St 14 3	0 2,3e+03 thermal, stem				
Use	Mobile Total Static Mode Energy Input and Output T Product Efficiency Use Location CO2 Footprint, source (kg) Power Rating (kW) Usage (hours per day) Usage (days per year)	ype Fossil fuel to vented sys 0.7 United St 14 3 30	0 2.3e+03 thermal stem				
Use	Mobile Total Static Mode Energy Input and Output T Product Efficiency Use Location CO2 Footprint, source (kg) Power Rating (kW) Usage (days per day) Usage (days per year) Product Life (years) Total Life Usage (hours)	ype Fossii fuel to vented syr 0.7 United St 14 3 30 5 4.5e+0	0 2.3e+03 thermal stem				
Use	Mobile Total Static Mode Energy Input and Output T Product Efficiency Use Location CO2 Footprint, source (kg) Power Rating (kW) Usage (hours per day) Usage (days per year) Product Life (years)	ype Fossii fuel to vented syr 0.7 United St 14 3 30 5 4.5e+0	0 2.3e+03 thermal stem		100		
nţ	Mobile Total Static Mode Energy Input and Output T Product Efficiency Use Location CO2 Footprint, source (kg) Power Rating (kW) Usage (days per day) Usage (days per year) Product Life (years) Total Life Usage (hours)	ype Fossii fuel to vented syr 0.7 United St 14 3 30 5 4.5e+0	0 2.3e+03 thermal stem	Potential En	100 Total Mass	Total EoL CO2 (kg)	%
Use End of Life	Mobile Total Static Mode Energy Input and Output T Product Efficiency Use Location CO2 Footprint, source (kg) Power Rating (kW) Usage (Idurs per day) Usage (Idays per year) Product Life (years) Total Life Usage (hours) Relative contributions of	ype Fossil fuel to vented system of the control of	0 2.3e+03 thermal. stem ates 8	Potential En of Life () 'Saving' (kg)	100 Total Mass		% 71.7
	Mobile Total Static Mode Energy Input and Output T Product Efficiency Use Location CO2 Footprint, source (kg) Power Rating (kW) Usage (hours per day) Usage (days per year) Product Life (years) Total Life Usage (hours) Relative contributions of	ype Fossil fuel to vented sy: 0.7 United St (J) 7.1e-0 14 3 30 5 4.5e+0 f end of life options End of Life Route	0 2.3e+03 thermal. stem ates 8 Collection CO2 (kg/kg	Potential En of Life (b) 'Saving' (kg/	d Total Mass	CO2 (kg)	71.7
nţ	Mobile Total Static Mode Energy Input and Output T Product Efficiency Use Location CO2 Footprint, source (kg) Power Rating (kW) Usage (hours per day) Usage (days per year) Product Life (years) Total Life Usage (hours) Relative contributions of Component	ype	0 2.3e+03 thermal.stem ates 8 Collection CO2 (kg/kg	Potential En of Life 'Saving' (kg/ g) -3.7	d Total Mass (kg)	CO2 (kg) -62	71.7
	Mobile Total Static Mode Energy Input and Output T Product Efficiency Use Location CO2 Footprint, source (kg) Power Rating (kW) Usage (hours per day) Usage (days per year) Product Life (years) Total Life Usage (hours) Relative contributions of Component Component 1 Component 2	ype	0 2.3e+03 thermal. stem ates 8 Collection CO2 (kg/kg 0.042 0.042	Potential En of Life 'Saving' (kg) '9'	d Total Mass (kg)	-62 -22	71.7

 $\ \, \text{Table 4. Detailed Breakdown of individual life phases: CO2} \, \textit{Foot Print} \, \text{-} \, \text{Patio Heater} \,$

5. Conclusion

The methods and tools presented in this book chapter, will guide in the design analysis of the role of materials and processes selection in terms of embodied energy, carbon foot print, recycle fraction, toxicity and sustainability criteria. A particular skills need to be used during the design process not only to satisfy the design requirements but also to minimize or eliminate adverse eco impacts (sustainable design). Two case studies of sustainable engineering and eco design are presented in this chapter book. The first case study deals with material selection for the condenser used in desalination plant and the second case study is about the life cycle analysis of patio heater. The results of the selection process for the heat exchanger (condenser) of a desalination plant show that the best material that can be used for the condenser is the stainless steel, duplex UNS S32255O, wrought. This material has (1) the highest design performance M (high heat flux), (2) the lowest cost (13 – 15 \$/Kg), (3) a very good resistance to pitting and crevice resistance, (4) an excellent resistance to stress corrosion cracking (no breaks at high strengths or > 75% of yield strength in various environments), (5) excellent material resistance to sea water (no degradation in material performance expected after a long exposure to sea water), and (6) a good pitting resistance equivalent number (PREN = 40). In addition the embodied energy (energy required to make 1 Kg of the material) and the CO2 foot print (mass of CO2 released during the production of 1 Kg of the material) are very low compared to the other materials. The second case study was about the life cycle analysis of the patio heater. The life cycle analysis strategy has two part: (1) an eco audit for a quick and approximate assessment of the distribution of energy demand and carbon emission over the patio heater's life; and (2) material selection to minimize the energy and carbon over the full life, balancing the influence of the choice over each phase of the life (selection strategies and eco informed material selection -suatianble design). The results of the life cycle analysis of patio heater show that the problem with the energy consumed and carbon foot print for the patio heater was during the use of the heater. A new materials can be selected to reduce the heat losses during the the use of the patio heater.

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The technological advancement of our civilization has created a consumer society expanding faster than the planet's resources allow, with our resource and energy needs rising exponentially in the past century. Securing the future of the human race will require an improved understanding of the environment as well as of technological solutions, mindsets and behaviors in line with modes of development that the ecosphere of our planet can support. Some experts see the only solution in a global deflation of the currently unsustainable exploitation of resources. However, sustainable development offers an approach that would be practical to fuse with the managerial strategies and assessment tools for policy and decision makers at the regional planning level. Environmentalists, architects, engineers, policy makers and economists will have to work together in order to ensure that planning and development can meet our society's present needs without compromising the security of future generations.

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